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# Multivariable Control Systems

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# References

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## References

- Multivariable Feedback Design, J M Maciejowski, Wesley, 1989.
- Multivariable Feedback Control, S. Skogestad, I. Postlethwaite, Wiley, 2005.

- تحلیل و طراحی سیستم های چند متغیره، دکتر علی خاکی صدیق

- کنترل مقاوم  $H_\infty$  ، دکتر حمید رضا تقی راد، محمد فتحی و فرینا زمانی اسگویی

# Introduction

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Topics to be covered include:

- ❖ Introduction
- ❖ Interaction
- ❖ Stability
- ❖ Analysis and design in multivariable systems
- ❖ Some examples of multivariable systems

# Introduction

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What is multivariable control?

MIMO systems are considered as multivariable systems.

A General multivariable plant

$$Y(s) = G(s)U(s)$$

$$Y(s) = \begin{bmatrix} y_1(s) \\ y_2(s) \\ \vdots \\ y_l(s) \end{bmatrix}$$

$$G(s) = \begin{bmatrix} g_{11}(s) & g_{12}(s) & \cdots & g_{1m}(s) \\ g_{21}(s) & g_{22}(s) & \cdots & g_{2m}(s) \\ \vdots & \vdots & \ddots & \vdots \\ g_{l1}(s) & g_{l2}(s) & \cdots & g_{lm}(s) \end{bmatrix}$$

$$U(s) = \begin{bmatrix} u_1(s) \\ u_2(s) \\ \vdots \\ u_m(s) \end{bmatrix}$$

Why they are different from SISO?

Since of interaction and design procedure.

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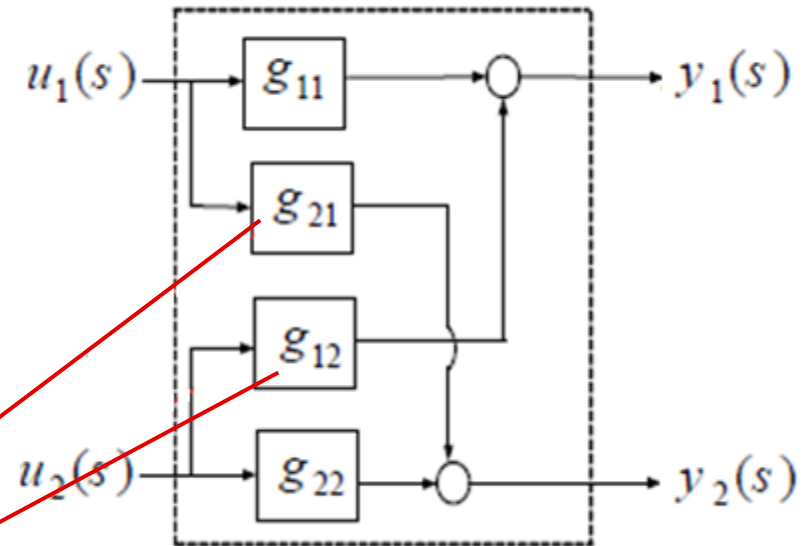
# Interaction

$$G(s) = \begin{bmatrix} g_{11}(s) & g_{12}(s) \\ g_{21}(s) & g_{22}(s) \end{bmatrix}$$



$$y_1(s) = g_{11}(s)u_1(s) + g_{12}(s)u_2(s)$$

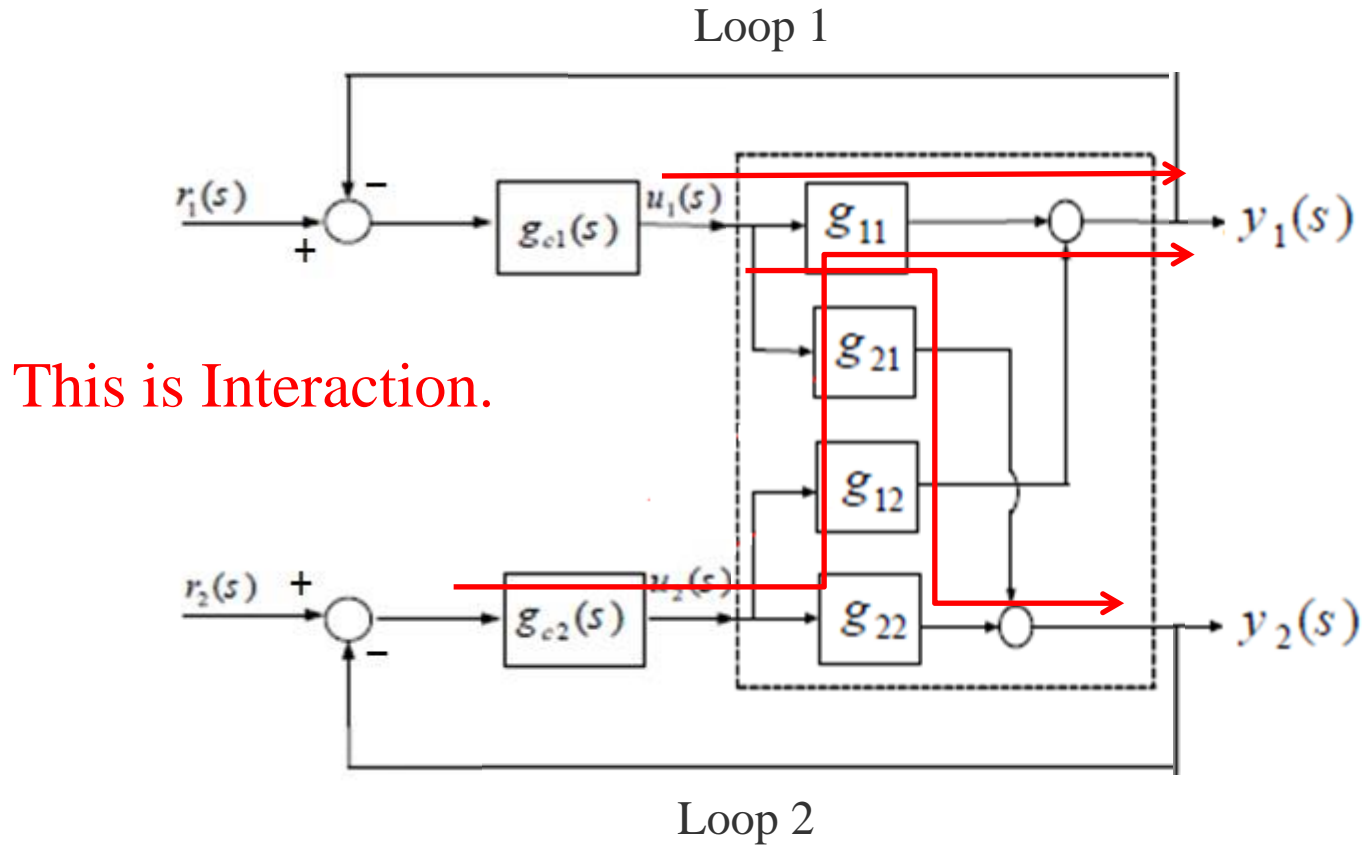
$$y_2(s) = g_{21}(s)u_1(s) + g_{22}(s)u_2(s)$$



Interaction

# Interaction

## Interaction on a system



**Direct effect:** The first controller will get the first output ....

**Indirect effect:** The first controller will disturb the second output and ....

# Interaction

One way or single direction interaction (Neutralization process)

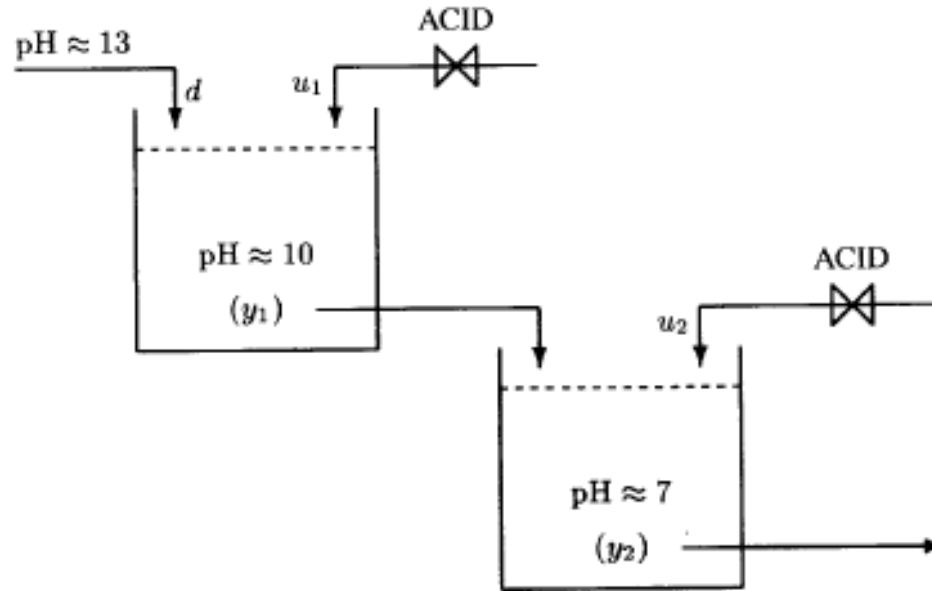
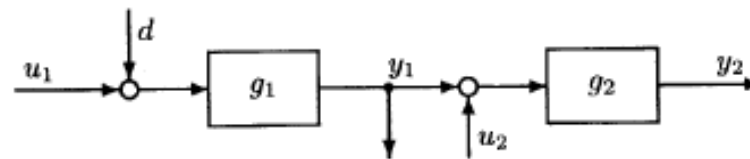


Figure B.1: Neutralization process

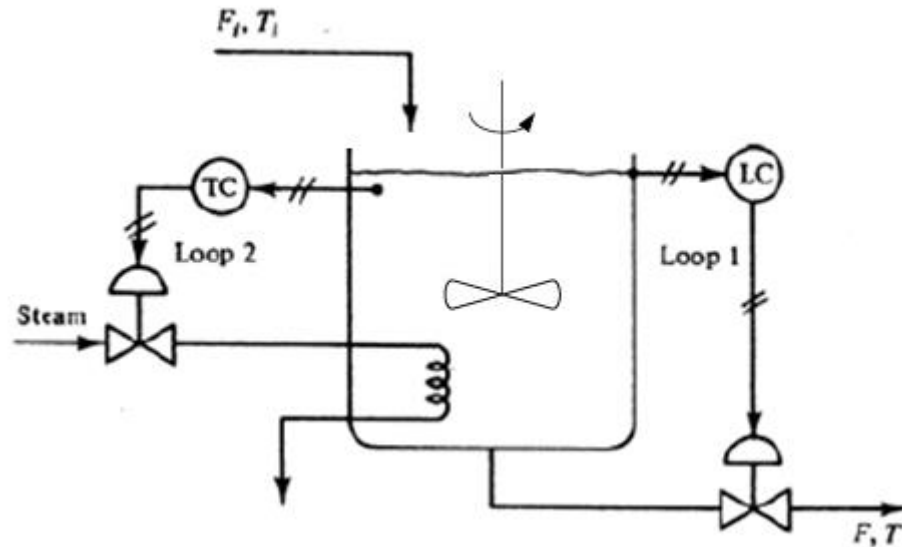


$$G(s) = \begin{bmatrix} g_1(s) & 0 \\ g_2(s)g_1(s) & g_2(s) \end{bmatrix}$$



# Interaction

One way or single direction interaction (Stirred tank heater)



$y_1$  is the level of tank.

$y_2$  is the temperature of tank.

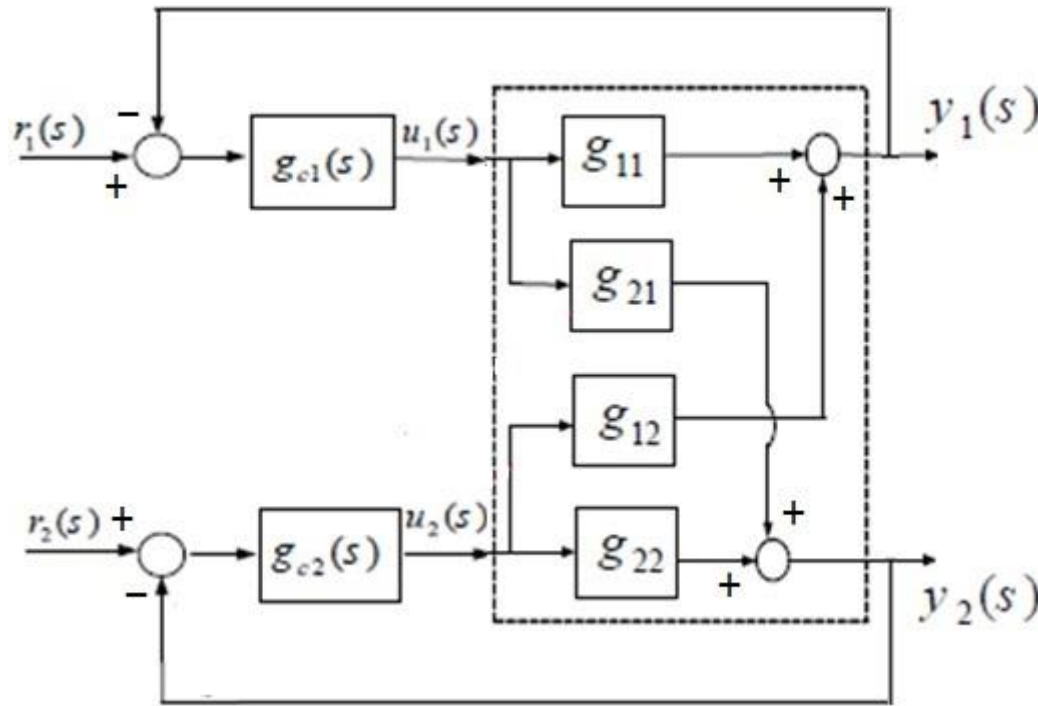
$$G(s) = \begin{bmatrix} g_{11}(s) & 0 \\ g_{21}(s) & g_{22}(s) \end{bmatrix}$$

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- ❖ **Stability**
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# Stability



$$\begin{aligned}\Delta(s) &= \\ &= 1 - (-g_{11}(s)g_{c1}(s) - g_{22}(s)g_{c2}(s) \\ &\quad + g_{12}(s)g_{21}(s)g_{c1}(s)g_{c2}(s)) \\ &\quad + (g_{11}(s)g_{c1}(s)g_{22}(s)g_{c2}(s))\end{aligned}$$

$$t_{12}(s) = \frac{g_{12}(s)g_{c2}(s)}{\Delta(s)}$$

$$t_{21}(s) = \frac{g_{21}(s)g_{c1}(s)}{\Delta(s)}$$

$$t_{11}(s) = \frac{g_{11}(s)g_{c1}(s) + g_{c1}(s)g_{c2}(s)(g_{11}(s)g_{22}(s) - g_{12}(s)g_{21}(s))}{\Delta(s)}$$

$$t_{22}(s) = \frac{g_{22}(s)g_{c2}(s) + g_{c1}(s)g_{c2}(s)(g_{11}(s)g_{22}(s) - g_{12}(s)g_{21}(s))}{\Delta(s)}$$

For stability analysis (BIBO) in the case of no interaction ( $g_{12}(s)=g_{21}(s)=0$ ) check:

$$1 + g_{11}(s)g_{c1}(s) = 0 \quad \text{and} \quad 1 + g_{22}(s)g_{c2}(s) = 0$$

For stability analysis (BIBO) with interaction check:

$$\Delta(s) = 0$$

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# Analysis and design in multivariable systems

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## Analysis of Multivariable Systems

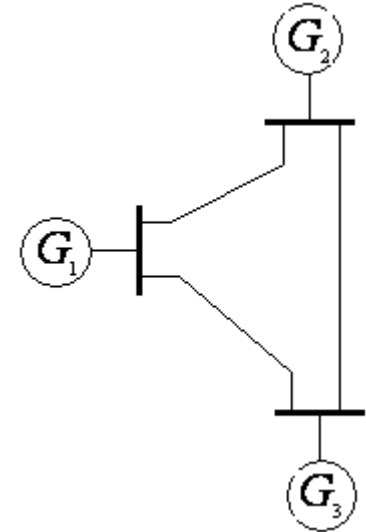
- Multivariable system representation
- Multivariable poles and zeros
- Controllability and observability
- State space realization
- Multivariable system stability
- Multivariable system robustness analysis
- Control structure design
- Control system design strategy 
  - Diagonal or decentralized
  - Block diagonal
  - Fully centralized

# Control system design strategy

Diagonal  
or  
decentralized

$$\begin{bmatrix} Ex_1 \\ Gov_1 \\ Ex_2 \\ Gov_2 \\ Ex_3 \\ Gov_3 \end{bmatrix} = \begin{bmatrix} * & 0 & 0 & 0 & 0 & 0 \\ 0 & * & 0 & 0 & 0 & 0 \\ 0 & 0 & * & 0 & 0 & 0 \\ 0 & 0 & 0 & * & 0 & 0 \\ 0 & 0 & 0 & 0 & * & 0 \\ 0 & 0 & 0 & 0 & 0 & * \end{bmatrix} \begin{bmatrix} V_{t1} \\ f_1 \\ V_{t2} \\ f_2 \\ V_{t3} \\ f_3 \end{bmatrix}$$

A multi machine power system



Block diagonal

$$\begin{bmatrix} Ex_1 \\ Gov_1 \\ Ex_2 \\ Gov_2 \\ Ex_3 \\ Gov_3 \end{bmatrix} = \begin{bmatrix} * & * & 0 & 0 & 0 & 0 \\ * & * & 0 & 0 & 0 & 0 \\ 0 & 0 & * & 0 & 0 & 0 \\ 0 & 0 & 0 & * & 0 & 0 \\ 0 & 0 & 0 & 0 & * & * \\ 0 & 0 & 0 & 0 & * & * \end{bmatrix} \begin{bmatrix} V_{t1} \\ f_1 \\ V_{t2} \\ f_2 \\ V_{t3} \\ f_3 \end{bmatrix}$$

Fully centralized

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# Analysis and design in multivariable systems

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## Multivariable Design Methodologies

- State space methods
- Multivariable root loci approach
- Rosenbrock frequency response approach or Robust approaches
- Pole placement methods
- Eigenstructure assignment
- Multivariable PID controllers
- The classical robust control methods
- QFT
- Soft computing approach

# Topics to be covered include:

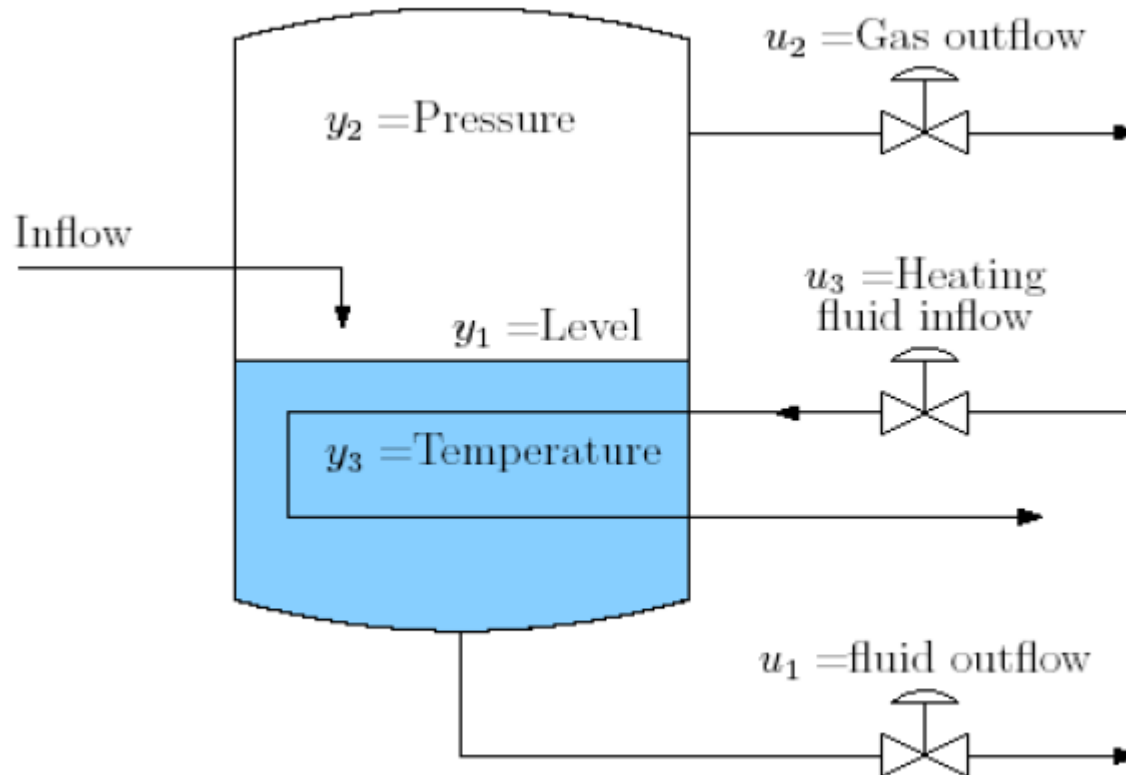
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- ❖ Introduction
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- ❖ Some examples of multivariable systems

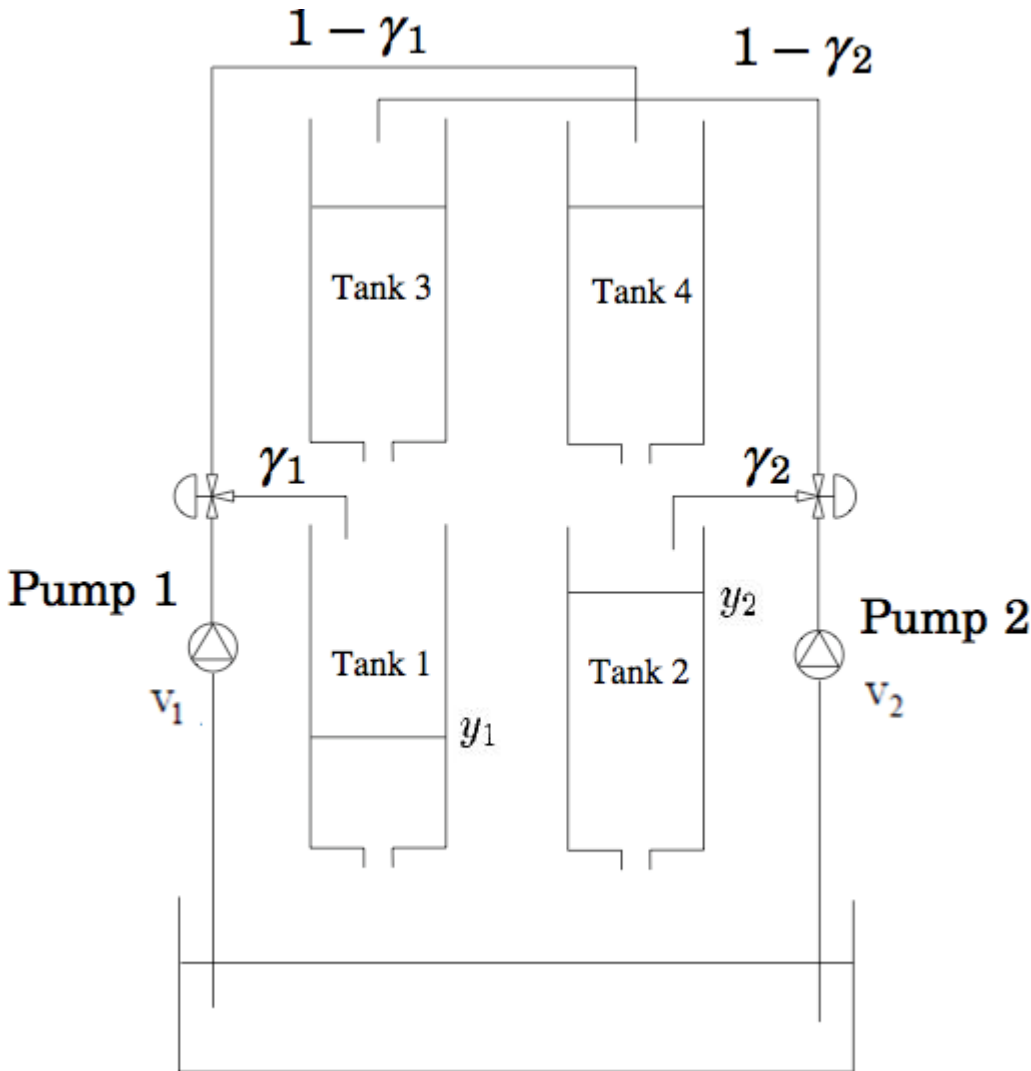


# Some examples of multivariable systems

A 3 inputs / 3 outputs chemical process



# Some examples of multivariable systems



$A_i$  - Cross sectional area of the tank ( $\text{m}^2$ )  
 $a_i$  - Cross sectional area of the outlet hole ( $\text{m}^2$ )  
 $h_i$  - Water level (m)  
 $k_i$  - valve coefficient

$$\frac{dh_1}{dt} = \frac{-a_1}{A_1} \sqrt{2gh_1} + \frac{a_3}{A_1} \sqrt{2gh_3} + \frac{\gamma_1 k_1}{A_1} v_1$$

$$\frac{dh_2}{dt} = \frac{-a_2}{A_2} \sqrt{2gh_2} + \frac{a_4}{A_2} \sqrt{2gh_4} + \frac{\gamma_2 k_2}{A_2} v_2$$

$$\frac{dh_3}{dt} = \frac{-a_3}{A_3} \sqrt{2gh_3} + \frac{(1-\gamma_2)k_2}{A_3} v_2$$

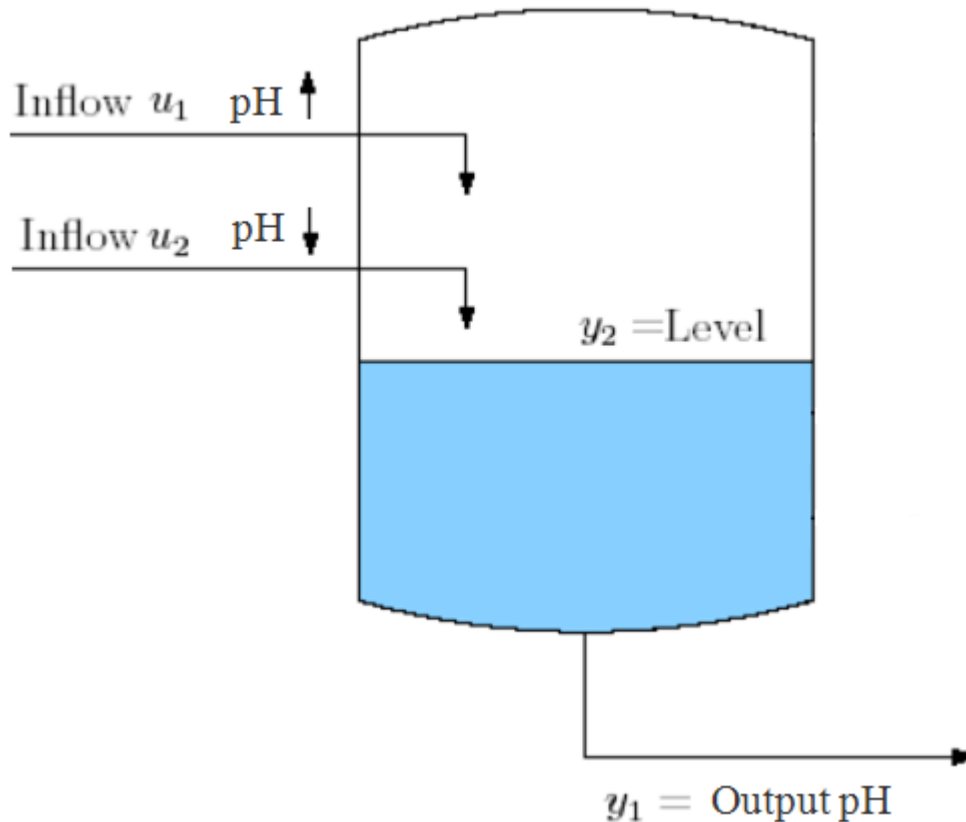
$$\frac{dh_4}{dt} = \frac{-a_4}{A_4} \sqrt{2gh_4} + \frac{(1-\gamma_1)k_1}{A_4} v_1$$

$\gamma_1 = \gamma_2 = 1$  No interaction.

$\gamma_1 = \gamma_2 = 0$  No interaction!?

# Some examples of multivariable systems

Example 1-1: Consider following two input two output system.



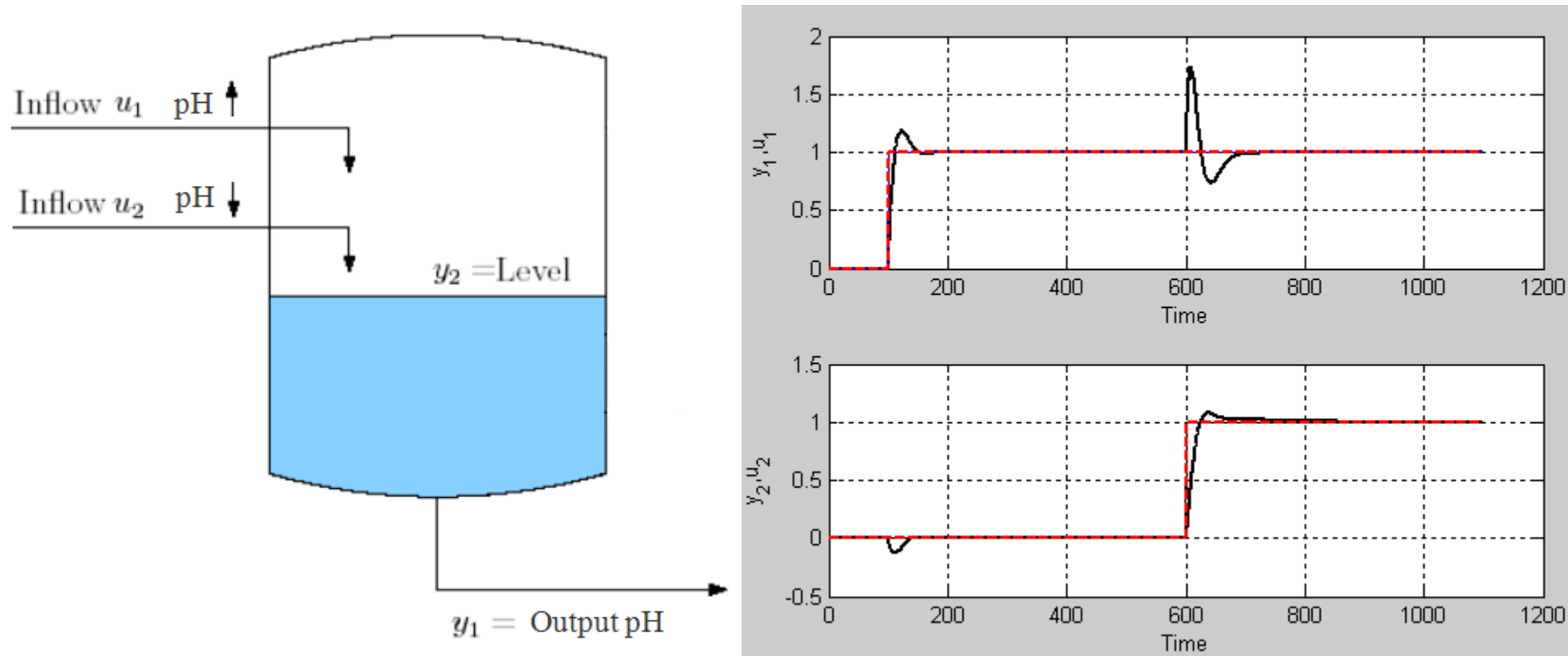
$$G(s) = \begin{bmatrix} \frac{-2.17}{85s+1} & \frac{2.13}{85s+1} \\ \frac{1}{175s+1} & \frac{1}{175s+1} \end{bmatrix}$$

Try a PI controller for  $g_{11}$

Try a PI controller for  $g_{22}$

$$G_c(s) = \begin{bmatrix} \frac{-5s - 0.2}{s} & 0 \\ 0 & \frac{8s + 0.1}{s} \end{bmatrix}$$

# Some examples of multivariable systems



**Exercise 1-1:** Derive Matlab code for above figure(m-file).

**Exercise 1-2:** Derive an MIMO example by yourself and explain it and do the same procedure as Example 1-1. (m-file is necessary).

# Exercises

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1-1 Mentioned in the lecture.

1-2 Mentioned in the lecture.

1-3 Derive a linear state space model for quadruple tank process.  
Let  $A_1=A_2=A_3=A_4=1$  and  $h_1=0.5$ ,  $h_2=0.6$ ,  $h_3=h_4=0.4$

1-4 Derive transfer function model for quadruple tank process around the linearized model.